

CME 265 Process Analysis Midterm 1 February 9, 2011

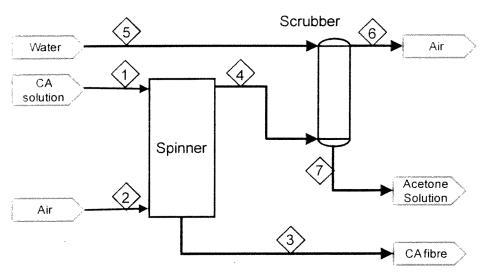
The exam is 50 minutes long.

Approved programmable calculators, textbooks and one 8.5x11" crib sheet permitted.

Do ALL questions and provide all answers on the question sheet.

Observe standard notation and problem solving methods for all solutions.

1. In the steady state spinning process shown below, cellulose acetate fibres (CA, stream 3) are spun from a solution of CA and acetone (stream 1). The liquid fibres are dried with warm air (stream 2), and all of the acetone leaves with the air (stream 4). The majority of the acetone is absorbed into water (stream 5) in a scrubber, and recycled back to the process for acetone recovery (stream 7). The exiting air contains a small percentage of acetone (stream 6) which is neglected for the moment.



Air: M=29; SG is unknown

Acetone (C₃H₆O): M=58; SG=0.791

Cellulose Acetate: molar mass and SG are unknown

Material Balance Table: Mass Basis SS, no rxn: IN=OUT

Component	1	2	3	4	5 6		7
Cellulose acetate (CA)	0.20	**	1.0	sas .	**	384	**
Acetone (S)	0.80	***	Adm	xs4=0.333	adhi	***	X87
Air (A)	wine Service S	1.0	1692	X14=0.667	Alfabet American and American Community (American American America	1.0	*
Water			-		1.0	440	Xw7
Flow (T/day)	50	\mathbf{F}_{2}	\mathbf{F}_3	F ₄	2	F ₆	F ₇

NAME

a) (10 points) Stream 4 is 20 mole percent acetone. Convert this composition to a mass basis, and enter the result in the material balance table.

For 100 mol Stream 4

Acetone 9mol M mass (g) mass fraction

Acetone 70 58 1160 0.333

Air 80 29 2370 0.667

b) (10 points) Now that you have solved for the stream 4 composition, complete a degrees of freedom analysis on the process. If you were not able to solve part (a), use x_{S4} =0.20 and x_{A4} =0.80.

Process step	Spin	Scrubber	Overall
Streams	1,2,3,4	4,5,6,7	1,2,3,5,6,7
Unknowns	3	5	6
Material Balances	3	3	4
$\sum x_i$	**Constanting**	1	1
Process Spec	digipanena	generalisment	0
Basis	Obstantinasco -	gga-minimakingg	0
Degrees of freedom	O	Agenticated and the second and the s	Y Simon Market Control of the Contro

c) (5 points) What vessel(s) or process step(s) should be chosen as the starting point for the material balance solution? Why?

The spinner because degrees of freedom = 0 so # equations = # unknowns.

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A	*	-				

d) (10 points) Write the material balances and other equations which apply to the spinner, and solve as many as possible.

$$= 0.67 \left[\frac{0.80}{0.33} \left(\frac{50T}{day} \right) \right] * F_2 = 160 \frac{7}{day}$$

$$= \frac{1207}{day} : F_4 = 120 \frac{7}{day}$$

$$= \frac{1207}{day} : F_4 = 120 \frac{7}{day}$$

e) (15 points) Complete the material balances for the rest of the process, solving for all remaining unknowns.

$$4N7 = \frac{2}{42} = 0.0476$$

$$787 = \frac{40}{42} = 1 - 0.0476 = 0.9524$$

$$Ex \neq 1$$
 -1 $x_{w7} = 0.05$ 5

Figure interpret ducto ECF -1 $x_{s7} = 0.95$ 5

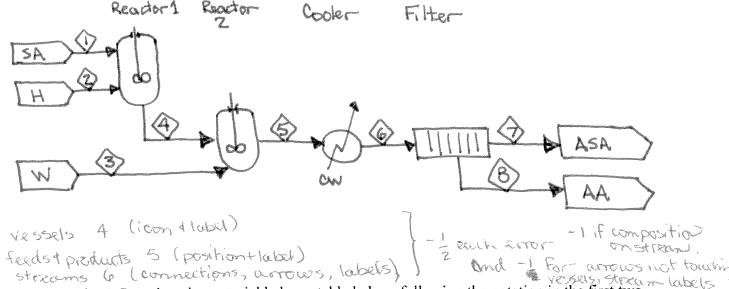
(must have contact for full years) $x_{s7} = 0.95$ 5

For full years) $x_{s7} = 0.95$

$$x_{w7} = 0.05$$
 $x_{s7} = 0.95$

NAME

- 2. The production of acetylsalicylic acid involves two reaction stages, cooling, and a final filtration step. In the first stirred tank reactor, two feed streams (crystalline salicylic acid (SA), and pure acetic anhydride (H)) are combined at 70°C. The product stream from the first reactor contains some unreacted H and the products acetylsalicylic acid (ASA) and acetic acid (AA). This stream is fed to a second stirred tank reactor, where fresh water (W) is added and the remaining H reacts to completion, giving a liquid product stream of ASA and AA. The product stream from the second reactor is cooled in a heat exchanger to crystalize the ASA out of solution, and then filtered to separate the wet ASA crystals from the liquid AA byproduct.
 - a) (15 points) Draw a flowsheet of the process using best practices and equipment icons.

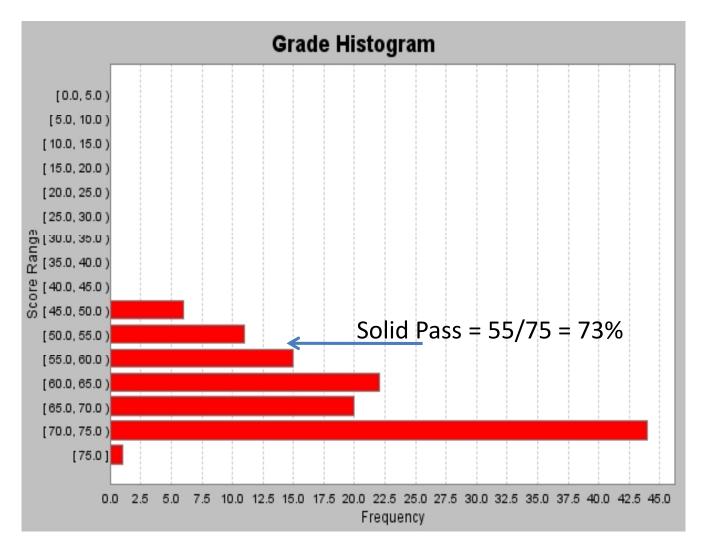


b) (10 points) Complete the material balance table below, following the notation in the first two streams. If a component is present, insert the appropriate x_{ij} variable. Otherwise, insert a dash (-). The stream numbers must match your flowsheet above: add or delete columns if necessary.

Component	1	2	3	4	5	6	7 2	8 7	9
SA	X _{SA,1}		_{ad} colonidations	- Constitution in the Cons	And the state of t	govinsk	gestions	Blessminnering	The state of the s
H		X _{H,2}	The second secon	X _{H4}	- Spanners	· Application	all-constal [®]	Browner	
W			Xw3		¥ Xw5	×~6	X _{W7}	Xwe	
ASA		1000	quartificities;	XASAA	X _{ASA5}	XASAG	X _{ASA} X		
AA	Allen	19406	mediage	XAAA	X445	X _{AA5}	XAA7	Ywas	Microphalas didycycyconias cyclysol
Flow	$\mathbf{F_{1}}$	F ₂	F ₃	F ₄	F ₅	$\mathbf{F_6}$	F ₇	F ₈	F

* If water is fed in excess, Xws to Xws are non-zero. Since one of the products is acetic aced, this is the most likely outcome.

* The water does not leave as a pure stream from any of the vessels,



Average: 64

Median: 67

Max: **75** Min: **46**

Count: **119** Std Dev: **8**

Clear Pass: 55/75

(no D's in this course! - MT1<50/75=F*0.15)

A range >70/75 (45/120 students!)